

## Lecture 13

### Flame Temperature

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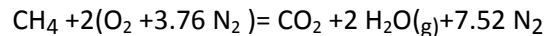
Exercise-3

**Key words: Flame temperature, Combustion, furnaces**

#### Exercise- 1 Flame temperature with theoretical air

Calculate theoretical maximum adiabatic flame temperature of fuel gas of composition 96 % CH<sub>4</sub>, 0.8 % CO<sub>2</sub> and 3.2 % N<sub>2</sub> when burnt with theoretical air. Assume fuel and air are mixed at 25°C

Consider 1 mole of fuel gas



POC    Amount (kg mole)

CO<sub>2</sub>    0.968

H<sub>2</sub>O    1.920

N<sub>2</sub>    7.52

Heat balance: Reference Temperature 25°C Or 298 k.

Sensible heat in air & fuel + Heat of combustion = Heat in products of combustion 1)

Sensible heat of reactants = 0 since they are Supplied 25°C .

$$-\Delta H_{298}^{\text{Comb.}} = 0.968 (94.05 \times 10^3) + 1.920 (57.80) \times -10^3 [ 0.96 \times 17.89] \times 10^3 = 184 \times 10^3 \text{ kcal.} \quad \text{----- (2)}$$

This heat of combustion raises the temperature of POC to the flame temperature.

The heat capacity of POC i. e. Cp'

$$\text{Cp}' = n \text{ CO}_2 \text{ C}_p \text{ CO}_2 + n \text{ H}_2 \text{ O C}_p \text{ H}_2\text{O} + n \text{ N}_2 \text{ C}_p \text{ N}_2$$

Where  $n_{CO_2}$ ,  $n_{N_2}$  and  $n_{H_2O}$  are moles of  $CO_2$ ,  $N_2$ ,  $H_2O$  respectively.

$$C_p^1 = 0.968 \left( 10.55 + 2.16 \times 10^{-3} T - \frac{2.04 \times 10^5}{T^2} \right) + 1.92 \left( 7.17 + 2.56 \times 10^{-3} T + \frac{0.08 \times 10^5}{T^2} \right) + 7.25 \left( 6.66 + 1.02 \times 10^{-3} T \right) = 72.27 + 14.41 \times 10^{-3} T - \frac{2.11 \times 10^5}{T^2} \frac{\text{kcal}}{\text{kg mole}^{\circ}\text{K}} \quad (3)$$

By 1 and 3

$$184 \times 10^3 = \int_{298}^{T_f} c_p^1 P dT \quad (4)$$

By 3 and 4

$$184 \times 10^3 = \int_{298}^{T_f} \left( 72.27 + 14.41 \times 10^{-3} T - \frac{2.11 \times 10^5}{T^2} \right) dT$$

Solution gives  $T_f = 2300\text{K}$ .

Consider the use of expression  $C_p = a + bT$  and recalculating flame temperature. Calculating  $C_p^1$  and making heat balance gives

$$0.0072 T_f^2 + 72.27 T_f - 206157 = 0.$$

This is a quadratic equation whose solution gives

$$T_f = 2319 \text{ K}.$$

Let us calculate flame temperature by using average  $C_p$  values of POC. Average  $C_p$  values of POC are given in lecture 12.

$$184000 = 0.96 \times 12.5 (T_f - 25) + 1.92 \times 7.73 (T_f - 25) + 7.12 \times 7.25 (T_f - 25)$$

Solution gives  $T = 2643\text{K}$ .

We note that the accuracy of calculation depends on  $C_p$  values. For accurate calculations  $C_p = a + bT + c/T^2$  must be used. However using  $C_p = a + bT$ , though simplifies calculation but flame temperature is slightly greater (a difference of 20 K in this example). Use of average  $C_p$  values though simplifies the flame temperature calculation but calculated flame temperature is greater than earlier ones.

## Exercise 2. Effect of excess air on AFT

Consider the fuel in 1. Now it is burnt with a) 20% excess air and b) 50% excess air calculate AFT in each case.

In the following calculations we will be using

$$C_p = a + b T$$

However, readers may perform calculation using

$$C_p = a + bT + c/T^2$$

Take 20% excess air

Amount of POC:  $\text{CO}_2 = 0.968$

$\text{H}_2\text{O} = 1.92$

$\text{O}_2 = 0.40$

$\text{N}_2 = 9.056$

We can calculate

$$C_p^1 = 87.18 + 16.11 T \text{ (kcal /kg mol)}$$

Heat of combustion =  $184 \times 10^3$  kcal.

Heat balance

$$184000 = \int_{298}^{T_f} (87.18 + 16.11T) dT$$

Integration yields

$$184000 = 87.18 T_f - 25979.6 + 8.05 \times 10^{-3} T_f^2 - 715.3$$

Rearrangement.

$$8.05 \times 10^{-3} T_f^2 + 87.18 T_f - 210695 = 0$$

$T_f = 2034$  K.

Similarly for 50% excess

POC:  $\text{CO}_2 = 0.968$

$\text{H}_2\text{O} = 1.92$

$\text{O}_2 = 1.0$

$$N_2 = 11.31$$

Heat balance yields.

$$9.18 \times 10^{-13} T_f^2 + 102.88 T_f - 215474 = 0$$

$$T_f = 1819 \text{ K}$$

We note that increase in excess air decreases flame temperature. This is due to increase in  $N_2$  and  $O_2$  in the POC.

Similar calculations can be done by enriching air with  $O_2$ .

### Exercise-3:

Calculate AFT when producer gas of composition 22.4% CO 12.6%  $CO_2$  and 65%  $N_2$  is burned with theoretical air. The air and producer gas enter at  $250^\circ\text{C}$ .

**Hint** Heat balance would be

Sensible heat in air + sensible heat in producer gas + heat of combustion = sensible heat in POC.

**Steps:**

1. Calculate composition of POC
2. Calculate sensible heats in air and POC
3. Calculate heat of combustion
4. Do heat balance and find AFT.

**Ans**  $T_f = 1472.5^\circ\text{C}$  when  $C_p = a + bT$  is used

Assignment

- 1) Calculate AFT when producer gas of composition 22.4% CO 12.6%  $CO_2$  and 65%  $N_2$  is burned with theoretical air. The air and producer gas enter at  $250^\circ\text{C}$ .

2) Calculate the adiabatic flame temperature for combustion of blast furnace gas analyzing 24% CO 12% CO<sub>2</sub>, 4% H<sub>2</sub> and 60% N<sub>2</sub> under the following conditions

- When theoretical air is used
- When air is 30% excess than theoretical
- When 30% excess air is preheated to 227<sup>o</sup>C and 327<sup>o</sup>c

3) Calculate theoretical maximum adiabatic flame temperature of fuel gas of composition 96 % CH<sub>4</sub>, 0.8 % CO<sub>2</sub> and 3.2 % N<sub>2</sub> when burnt with theoretical air. Assume fuel and air are mixed at 25<sup>o</sup>C